

OXIDATION KINETICS OF MIXTURES OF *ISO*-OCTANE WITH ETHANOL OR BUTANOL IN A JET-STIRRED REACTOR: EXPERIMENTAL AND MODELING STUDY.

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Abstract

The kinetics of oxidation of mixtures of *iso*-octane with ethanol or 1-butanol (25/75, 50/50, and 75/25 % in vol.) were studied experimentally using a fused silica jet stirred reactor. The experiments were performed in the temperature range 770-1190 K, at 10 atm, at an equivalence ratio of 1. A kinetic modeling was performed using a reaction mechanism resulting from the merging of validated kinetic schemes for the oxidation of the components of the present mixtures (*iso*-octane, ethanol, and 1-butanol). Good agreement between the experimental results and the computations was observed under the present conditions. Reaction path analyses and sensitivity analyses were used to interpret the results.

Introduction

The increase of pollutants and carbon dioxide emissions from ground transportation engines operating with fossil fuels is a major concern [1-5]. Over the last two decades the inclusion of non-fossil fuel compounds was increasingly used to reduce carbon [6] and mixtures of a variety of oxygenates with petrol gasoline is frequently used. Among these oxygenates, ethanol is the most important gasoline component. However, its increasing use as a fuel raised concerns since relatively large amounts of ethanol and acetaldehyde may be present in engine exhausts [7-13]. More recently, 1-butanol was proposed for blending with gasoline, because of its high energy content (27 MJ/L compared to ≈ 21 MJ/L for ethanol) and its low vapor pressure (Reid values of 0.33 psi for 1-butanol compared to 2 psi for ethanol, and 4.5 psi for gasoline; 1 psi = 0.06894 bar) [14]. Moreover, the interest for producing butanol by advanced fermentation techniques is increasing [15-18]. For engine combustion experiments and modeling, simple surrogates are frequently preferred. In that contest, gasoline could be represented by *iso*-octane. Therefore, mixtures of *iso*-octane with alcohols could represent useful surrogates. However, only few studies concern the oxidation/combustion of such blends [19] whereas more studies concerned ethanol-gasoline [20-23] blends and butanol-gasoline blends [24-25]. These experiments did not provide the data needed for detailed kinetic modeling.

As part of a continuing effort in this laboratory to improve the knowledge of fuel combustion kinetics and provide the needed inputs for future modeling, we (i) performed experiments on the oxidation of mixtures of *iso*-octane with ethanol or 1-butanol in a jet-stirred reactor (JSR) and (ii) proposed a kinetic model for representing the data. The experimental and modeling results obtained in the present study are reported in the next sections. They are complementary to those published earlier for the kinetics of oxidation of E85 and Butanol85 where the gasoline fraction was represented by a more complex mixture of *iso*-octane, 1-hexene, and toluene [26-27].

Experimental

A fused-silica spherical jet-stirred reactor (JSR) operating at 10 atm was used. It is similar to that used previously [27-28]. It was located inside a regulated electrical resistance oven of ≈ 1.5 kW wrapped with insulating ceramic wool and enclosed in a stainless steel pressure-resistant jacket. Ethanol (99.8% pure, Aldrich), 1-Butanol (99% pure, Aldrich) and *iso*-octane ($>99.7\%$ pure, Aldrich) were mixed after thorough ultrasonic degassing. The liquid fuel mixture was pumped, using a micro piston HPLC pump (Shimadzu LC-120 ADvp) with an on-line degasser (Shimadzu DGU-20 A3). It was sent to an in-house stainless steel atomizer-vaporizer assembly maintained at 175 °C. A flow of nitrogen (50L/h) was used for the atomization. The oxygen (99.995% pure, Air Liquide) flow was diluted by a flow of nitrogen (<50 ppm of O₂; <1000 ppm of Ar; <5 ppm of H₂, Air Liquide). This oxygen-nitrogen flow was mixed with the fuel-nitrogen flow just before the entrance of the injectors, after preheating to a temperature close to that inside the JSR. All the gases were regulated by thermal mass-flow controllers (Brooks 5850E). Residence time distribution studies showed that under the conditions of the present study the reactor is operating under macro-mixing conditions [28]. As in previous work [27-29], thermocouple measurements (0.1 mm diameter Pt/ Pt-Rh 10% located inside a thin-wall fused-silica tube to avoid catalytic reactions on the wires) showed good thermal homogeneity along the vertical axis of the reactor. Typical temperature gradients of less than ≈ 2 K/cm were measured. Since the experiments were performed under high dilution, the temperature rise due to the reaction was generally lower than ≈ 30 K. Low pressure samples of the reacting mixtures were taken by sonic probe sampling and collected in 1 liter Pyrex bulbs at ≈ 40 mBar for immediate gas chromatography (GC) analyses as in [27, 29-30].

For the concentration measurements of hydrocarbons and oxygenates, capillary columns of 0.32 mm i.d. (DB-624, 50m and Al₂O₃/KCl 50m) were used with a flame ionization detector (FID) and helium as carrier gas. Hydrogen and oxygen were measured using a 0.53 mm i.d. capillary column (Carboplot, 25m) fitted to a thermal conductivity detector; nitrogen was used as carrier gas. Products identification was made by GC/MS. On-line Fourier transform infra-red (FTIR) analyses of the reacting gases were also performed by connecting the sampling probe to a temperature controlled gas cell (140 °C, 10 m path length, 0.5 cm⁻¹ resolution) via a Teflon heated line maintained at 175 °C. The sample pressure in the cell was 0.2 bar. This analytical equipment allowed the measurements of H₂, H₂O, O₂, CO, CO₂, CH₂O, CH₄, C₂H₆, C₂H₄, C₂H₂, ethanol, acetaldehyde, C₃H₆, 1-butanol, butanal, 1- and *iso*-C₄H₈, 1,3-C₄H₆, C₅H₁₀, and *iso*-octane. As previously [27, 29], very good agreement between the GC and FTIR analyses was found for the compounds measured by both techniques. Carbon balance was checked for every sample and found good (typically 100 \pm 8%).

Chemical Kinetic Modeling

The chemical kinetic modeling was performed using the PSR computer code of the Chemkin II library [31]. We used a kinetic reaction mechanism [27] obtained by merging the oxidation sub-scheme of ethanol and 1-butanol and a more general hydrocarbon combustion scheme. The resulting scheme (228 species and 1737 reactions) is available from the authors upon request (dagaut@cnrs-orleans.fr). The rate constants for the reverse reactions were computed from the forward rate constants and the appropriate equilibrium constants calculated using thermochemical data [27, 32-34]. To rationalize the results, sensitivity analyses and reaction rates analyses were performed. The rates of consumption (R with a negative sign) and production (R with a positive sign) for every species were computed.

Results and Discussion

The oxidation of ethanol-*iso*-octane and 1-butanol-*iso*-octane mixtures (25-75, 50-50, and 75-25 vol. %) was studied. The composition of the reacting mixtures is given in Table 1.

Table 1. Experimental conditions (residence time= 0.7s, pressure= 10 atm, 1500 ppm of fuel, stoichiometric mixtures, balance: nitrogen).

Alcohol- <i>iso</i> -octane (vol. %), <i>mixture</i>	Initial mole fractions			
	ethanol	1-butanol	<i>iso</i> -octane	oxygen
25-75, <i>A</i>	0.000728	0	0.000772	0.986664
50-50, <i>B</i>	0.001108	0	0.000392	0.008223
75-25, <i>C</i>	0.001342	0	0.000158	0.006003
25-75, <i>D</i>	0	0.000563	0.000937	0.015089
50-50, <i>E</i>	0	0.000965	0.000535	0.012477
75-25, <i>F</i>	0	0.001266	0.000234	0.010521

The oxidation of these mixtures was performed in a JSR at a fixed residence time of 0.7 s and at 10 atm. During the JSR experiments, 21 species were identified and measured by GC, FID, and TCD. Experimental mole fractions as a function of temperature were obtained for H₂, H₂O, O₂, CO, CO₂, CH₂O, CH₄, C₂H₆, C₂H₄, C₂H₂, ethanol, acetaldehyde (ethanal), C₃H₆, 1-butanol, butanal, 1- and *iso*-C₄H₈, 1,3-C₄H₆, C₅H₁₀ and *iso*-octane. No new species resulting from the interactions of the fuel components or their specific fragments could be measured. No cool flame could be observed in the present experiments in the temperature range 550-800 K, as expected since no such oxidation occurred with the fuel components under similar conditions [26, 35-37]. The experimental results showed that increasing the initial fraction of alcohol reduces the maximum mole fractions of formaldehyde, methane, and propene, but increases the formation of acetaldehyde and butanal (butanol case only). For ethanol blends, the formation of ethylene decreases with increasing ethanol content in the fuel whereas for butanol blends, the opposite behavior was observed. These trends could be explained using reaction paths analyses, as presented in the next paragraph.

Table 2. Maximum mole fractions of stable intermediates (residence time= 0.7s, pressure= 10 atm, 1500 ppm of fuel, and stoichiometric mixtures).

Alcohol- <i>iso</i> -octane (vol. %), <i>mixture</i>	Maximum mole fractions					
	CH ₂ O	CH ₃ CHO	butanal	CH ₄	C ₂ H ₄	C ₃ H ₆
25-75, <i>A</i>	2.36E-04	1.42E-04	na	6.31E-04	3.86E-04	1.59E-04
50-50, <i>B</i>	1.73E-04	2.02E-04	na	5.18E-04	3.08E-04	8.30E-05
75-25, <i>C</i>	1.37E-04	2.36E-04	na	3.61E-04	2.32E-04	3.41E-05
Variation (A to C)	–	+	na	–	–	–
25-75, <i>D</i>	3.05E-04	7.36E-05	7.62E-05	6.87E-04	4.95E-04	2.31E-04
50-50, <i>E</i>	2.83E-04	9.29E-05	1.16E-04	5.37E-04	5.02E-04	1.98E-04
75-25, <i>F</i>	2.61E-04	1.16E-04	1.64E-04	3.92E-04	5.37E-04	1.86E-04
Variation (D to F)	–	+	+	–	+	–

Figures 1 to 6 show comparisons between the present experimental and modeling results using the proposed detailed kinetic scheme. As can be seen from these figures, the model represents well the consumption of the fuels as well as the intermediate formation of hydrocarbons and oxygenates, and that of final products. It should be noted that the

intermediate formation of ethylene and methane is generally under-estimated by the model. Also, the maximum mole fraction of carbon monoxide is under-estimated by the model.

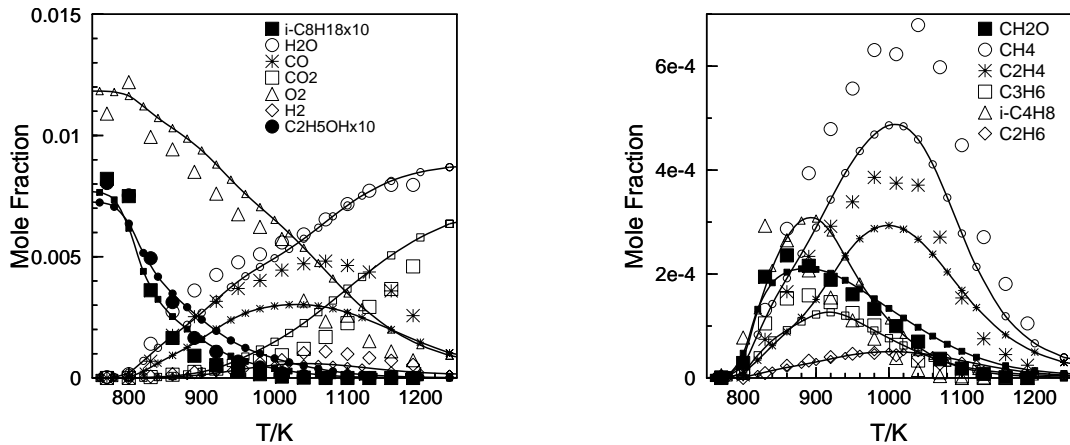


Figure 1. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture A (ethanol-*iso*-octane 25-75 vol.%) in a JSR.

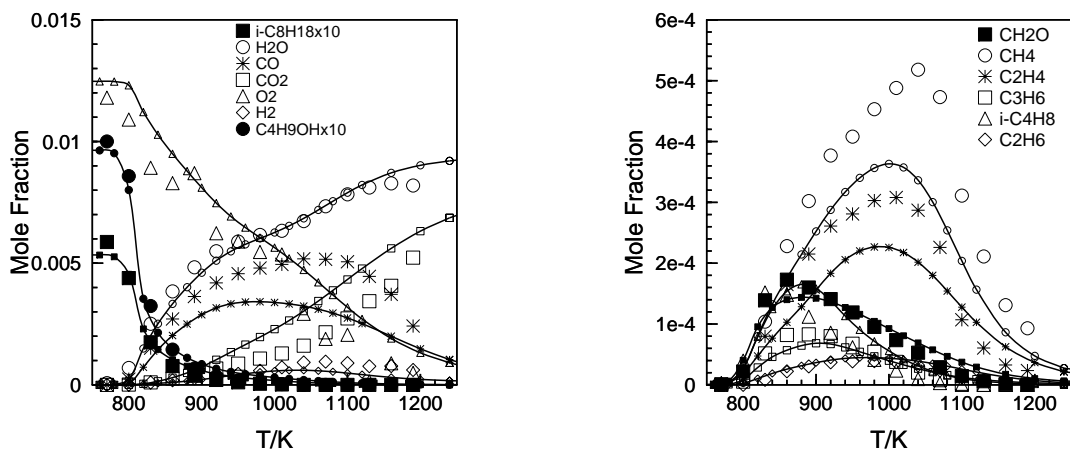


Figure 2. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture B (ethanol-*iso*-octane 50-50 vol.%) in a JSR.

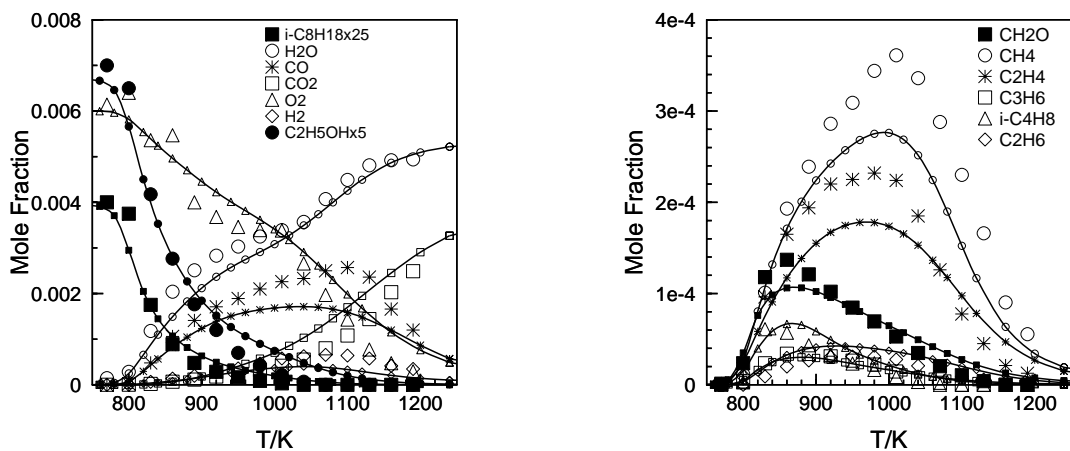


Figure 3. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture C (ethanol-*iso*-octane 75-25 vol.%) in a JSR.

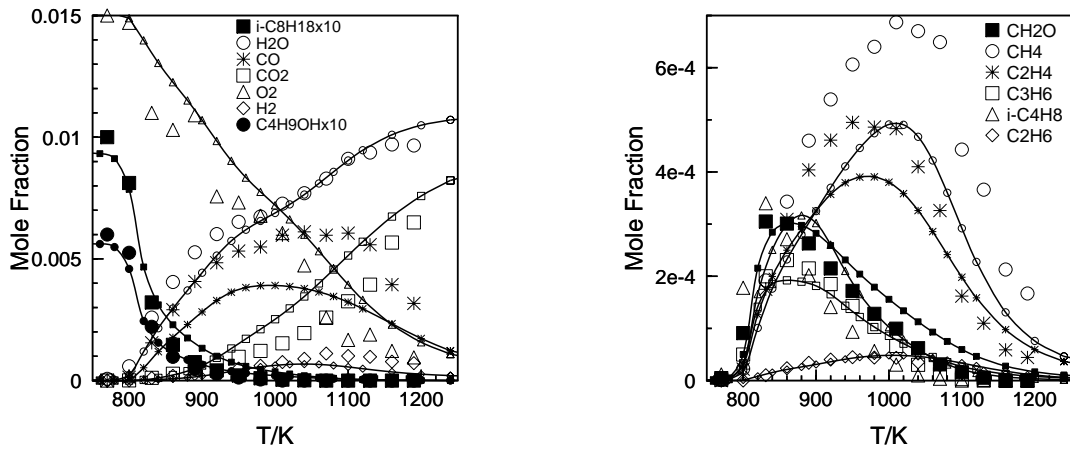


Figure 4. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture D (butanol-*iso*-octane 25-75 vol.%) in a JSR.

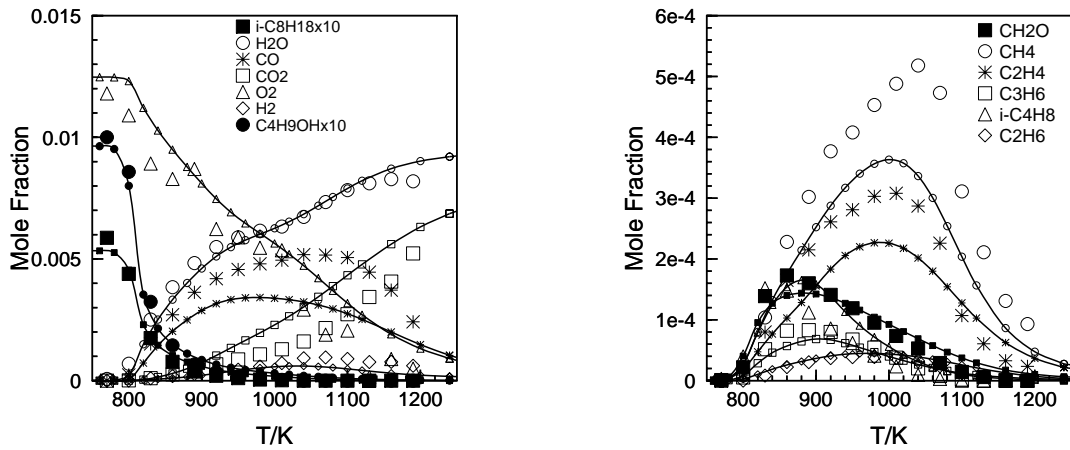


Figure 5. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture E (butanol-*iso*-octane 50-50 vol.%) in a JSR.

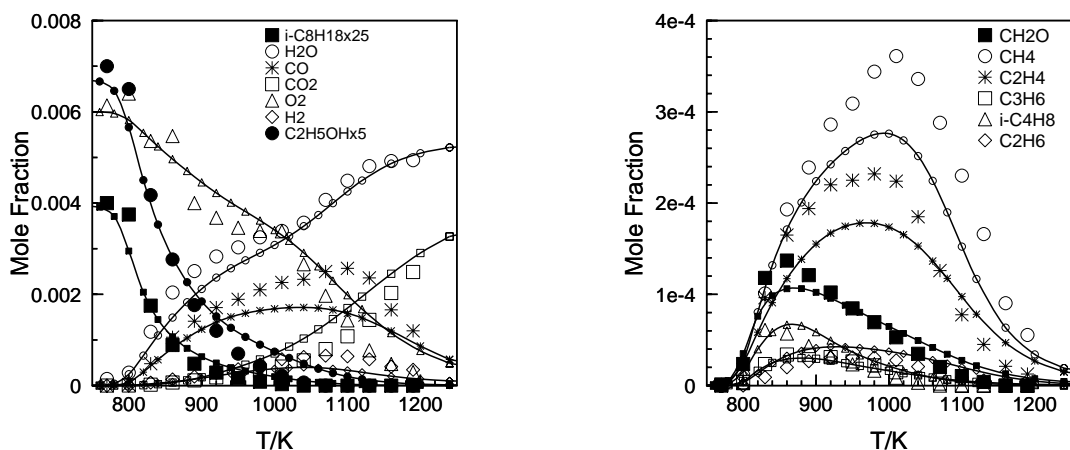


Figure 6. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of mixture F (butanol-*iso*-octane 75-25 vol.%) in a JSR.

This is due to uncertainties in the *iso*-octane sub-scheme, as demonstrated by modeling the oxidation of *iso*-octane under similar conditions (Figure 7). Nevertheless, reaction paths analyses, using the detailed chemical scheme, were performed to delineate the main oxidation reaction paths of the fuels. Normalized rates of production and consumption were computed for every species.

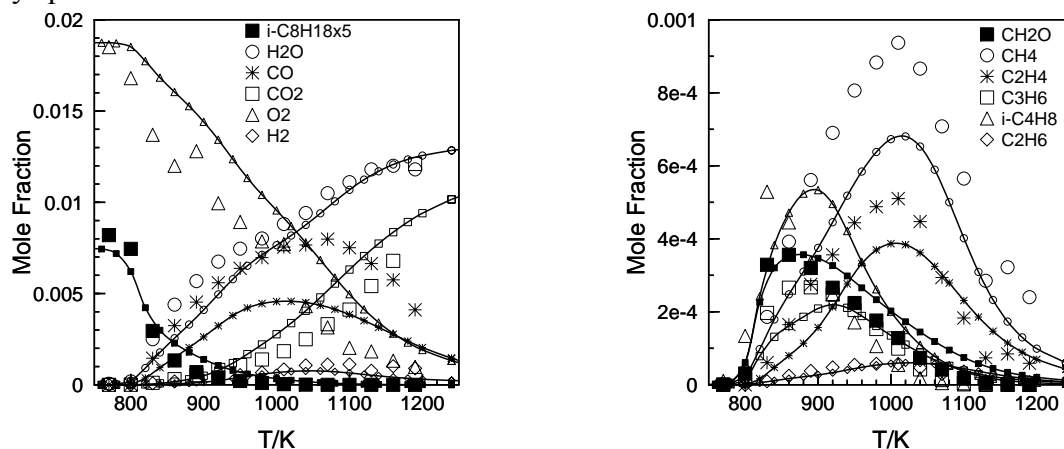
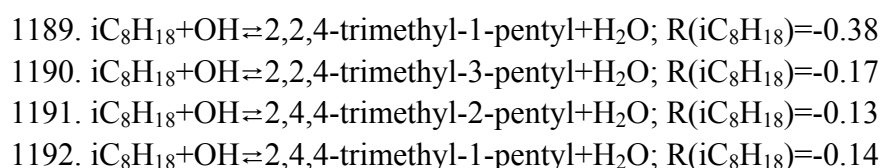
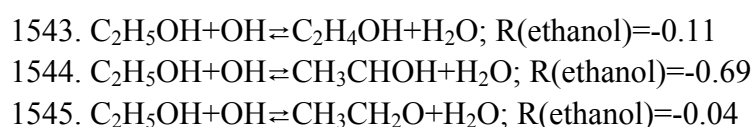


Figure 7. Comparison between experimental (large symbols) and computed (line and small symbol) results for the oxidation of *iso*-octane in a JSR (Mole fractions: *iso*-C₈H₁₈, 0.00150; O₂, 0.01875; N₂, 0.97975; residence time= 0.7s, pressure= 10 atm).

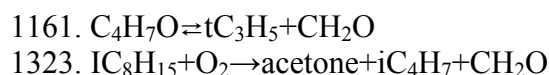
Reaction paths analyses were performed showing that for the ethanol-*iso*-octane fuel mixtures, *iso*-octane reacts predominantly via metathesis with OH (at 900 K, mixture A)



Ethanol is also mainly consumed via reaction with OH

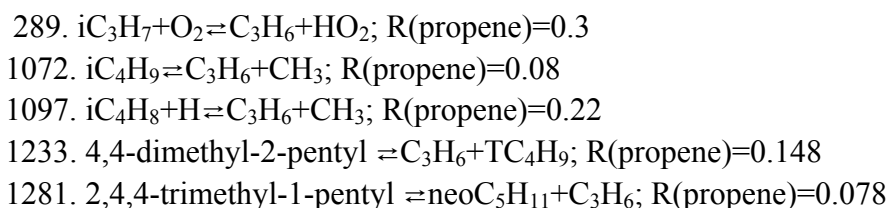


Increasing the initial fraction of ethanol reduces the maximum mole fractions of formaldehyde because its formation by decomposition of C₄H₇O and reaction of iC₈H₁₅ with O₂ get less important and slower.

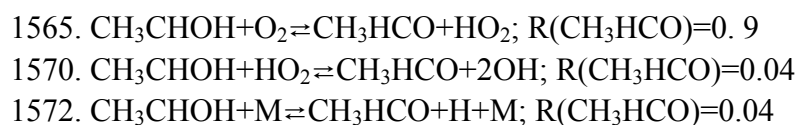


The rate of reaction 1161 is reduced by a factor of ≈ 4 and that of reaction 1323 by a factor of ≈ 11 when moving from mixture A to mixture C. Increasing the initial fraction of ethanol reduces the maximum mole fractions of methane because of the reduced rate of production of methyl radical (10% reduction), itself resulting from a lower concentration of *iso*-octane. Methane is mainly produced by reactions of methyl radicals with HO₂, CH₂O, iC₄H₈, and the fuel components. Increasing the initial fraction of ethanol reduces the maximum mole

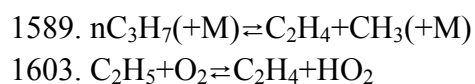
fractions of propene because propene production mostly results from the oxidation of *iso*-octane (at 900 K, mixture C):



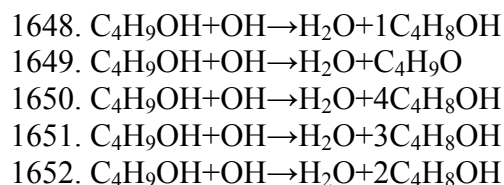
Increasing the initial fraction of ethanol increases the maximum mole fractions of acetaldehyde because ethanol readily produces acetaldehyde, as already reported [26] (at 900 K, mixture C):



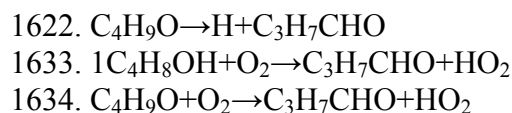
Increasing the initial fraction of ethanol decreases the maximum mole fractions of ethylene because ethanol produces very little ethylene by oxidation. Its formation occurs via



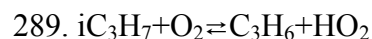
Reaction paths analyses were performed showing that for the butanol-*iso*-octane fuel mixtures, *iso*-octane reacts predominantly via metathesis with OH, as already described for the ethanol-*iso*-octane mixtures. Butanol is mainly consumed via metathesis with OH:

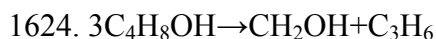


Increasing the initial fraction of butanol increases the maximum mole fractions of butanal because it is essentially formed by oxidation of butanol:

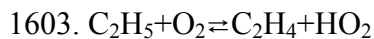
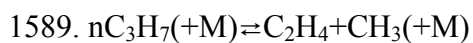


Increasing the initial fraction of butanol reduces the maximum mole fractions of formaldehyde for the same reasons as with the ethanol-*iso*-octane fuel mixture. Increasing the initial fraction of butanol reduces the maximum mole fractions of methane because of the reduced rate of production of methyl radical, itself resulting from a reduced concentration of *iso*-octane. Increasing the initial fraction of butanol reduces the maximum mole fractions of propene because of the reduced rate of production of *isopropyl* radicals through *iso*-octane oxidation, although propene is also produced by butanol oxidation:





Increasing the initial fraction of butanol (mixture D to F) increases the maximum mole fractions of ethylene as a result of the increased rates of reactions 1589 and 1603 by a factor of ≈ 2 :



Local, first-order sensitivity analyses were performed to delineate the most influencing reactions in the scheme.

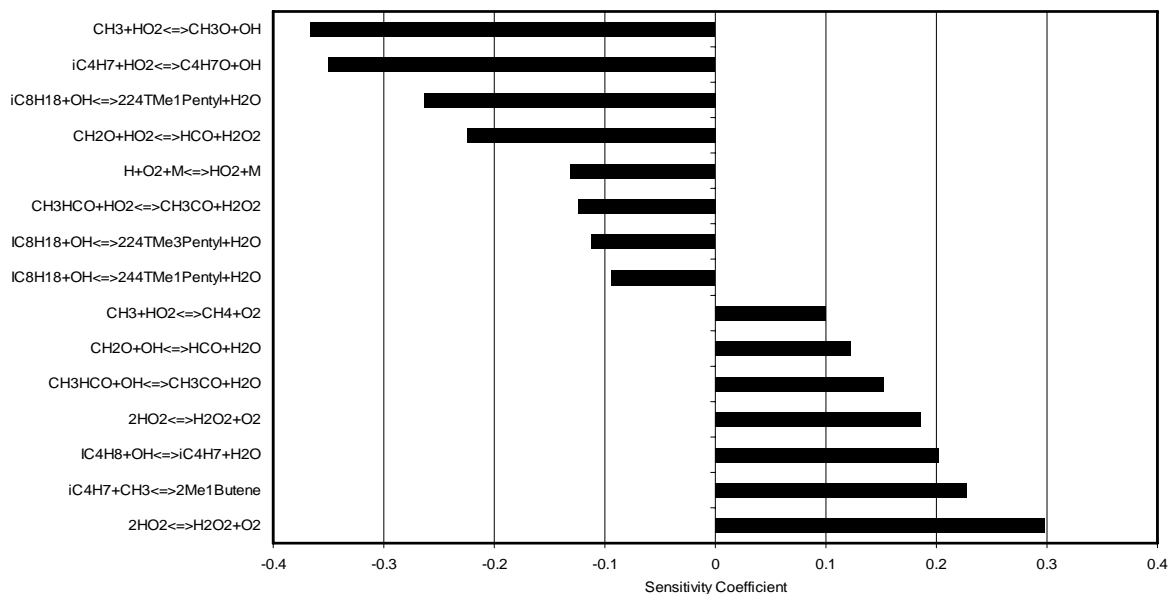


Figure 8. Sensitivity spectrum for *iso*-octane (Mixture B at 900 K, 10 atm, 0.7s).

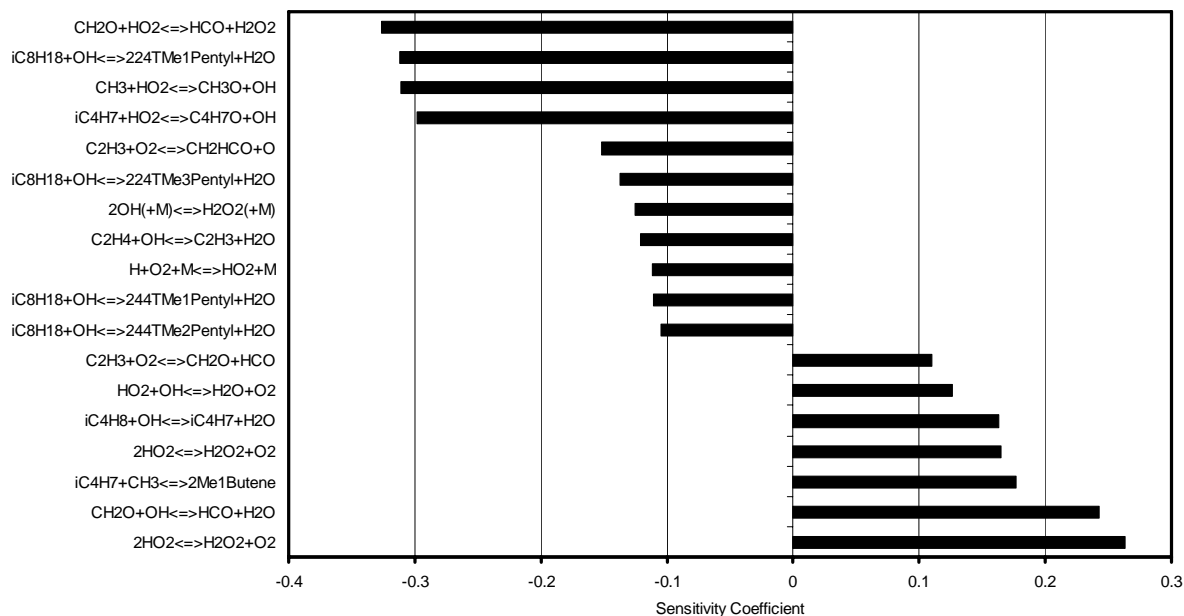


Figure 9. Sensitivity spectrum for *iso*-octane (Mixture E at 900 K, 10 atm, 0.7s).

As can be seen from Figures 8-9, the most sensitive reactions remain the same when ethanol or butanol is present in the fuel. However, the kinetics of reactions pertaining to the ethanol

sub-scheme also influences the model predictions since the following reactions have significant sensitivity coefficients:



By consuming OH radicals, reaction tends to reduce the rate of consumption of the fuel that mostly reacts with OH. Conversely, reaction 248 that produces H₂O₂ tends to favor the oxidation of the fuel since in turn, hydrogen peroxide decomposes to yield two OH radicals. The reaction $2 \text{HO}_2 \rightleftharpoons \text{H}_2\text{O}_2 + \text{O}_2$ appears twice because its complex temperature dependence required using two Arrhenius expressions.

Conclusion

The two main objectives of this study were achieved: (i) New data consisting of concentration profiles of reactants, stable intermediates, and final products were measured as a function of temperature for the oxidation of stoichiometric mixtures of ethanol and *iso*-octane and 1-butanol and *iso*-octane, in a JSR operating at 10 atm and 0.7s; (ii) A chemical kinetic modeling of these experiments was performed using a mechanism derived from previous work. Very similar reaction paths were observed when increasing the alcohol fraction in the fuel (25 to 75% vol.). As expected, increasing the initial fraction of alcohol in the fuel increases the importance of its reaction routes for the formation of the products measured here. Variations in products formation with changing fuel composition were rationalized through kinetic modeling.

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